

Module ChE 311 Biochemical Engineering

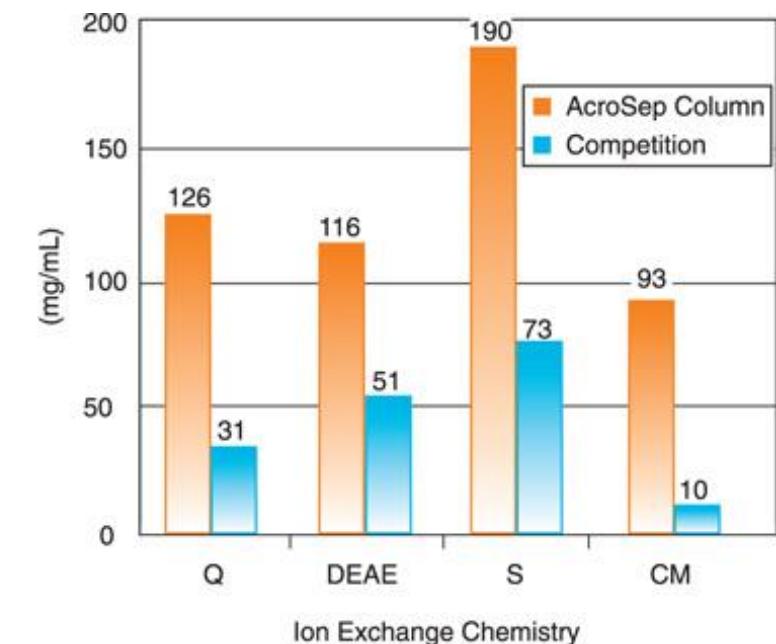
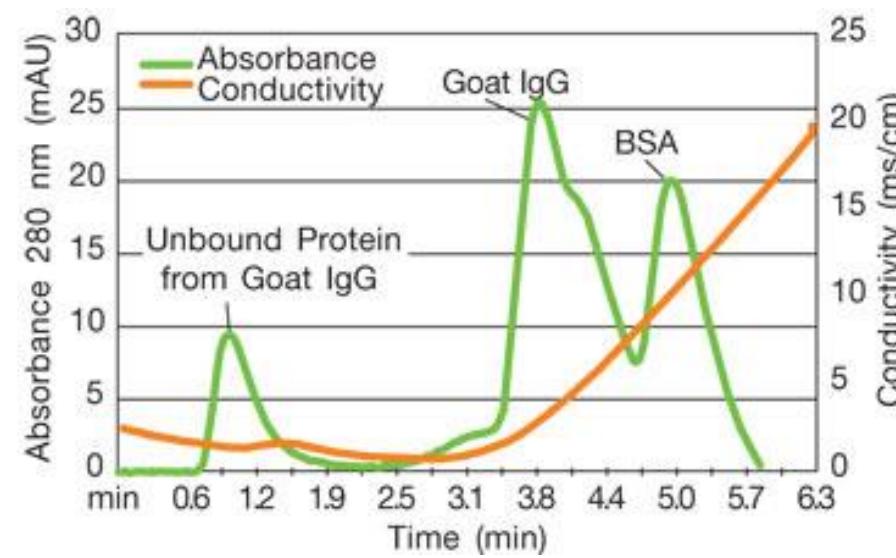
Downstream processing

Lecture 4B – Chromatography basics

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Chromatography (well, mostly protein chromatography)

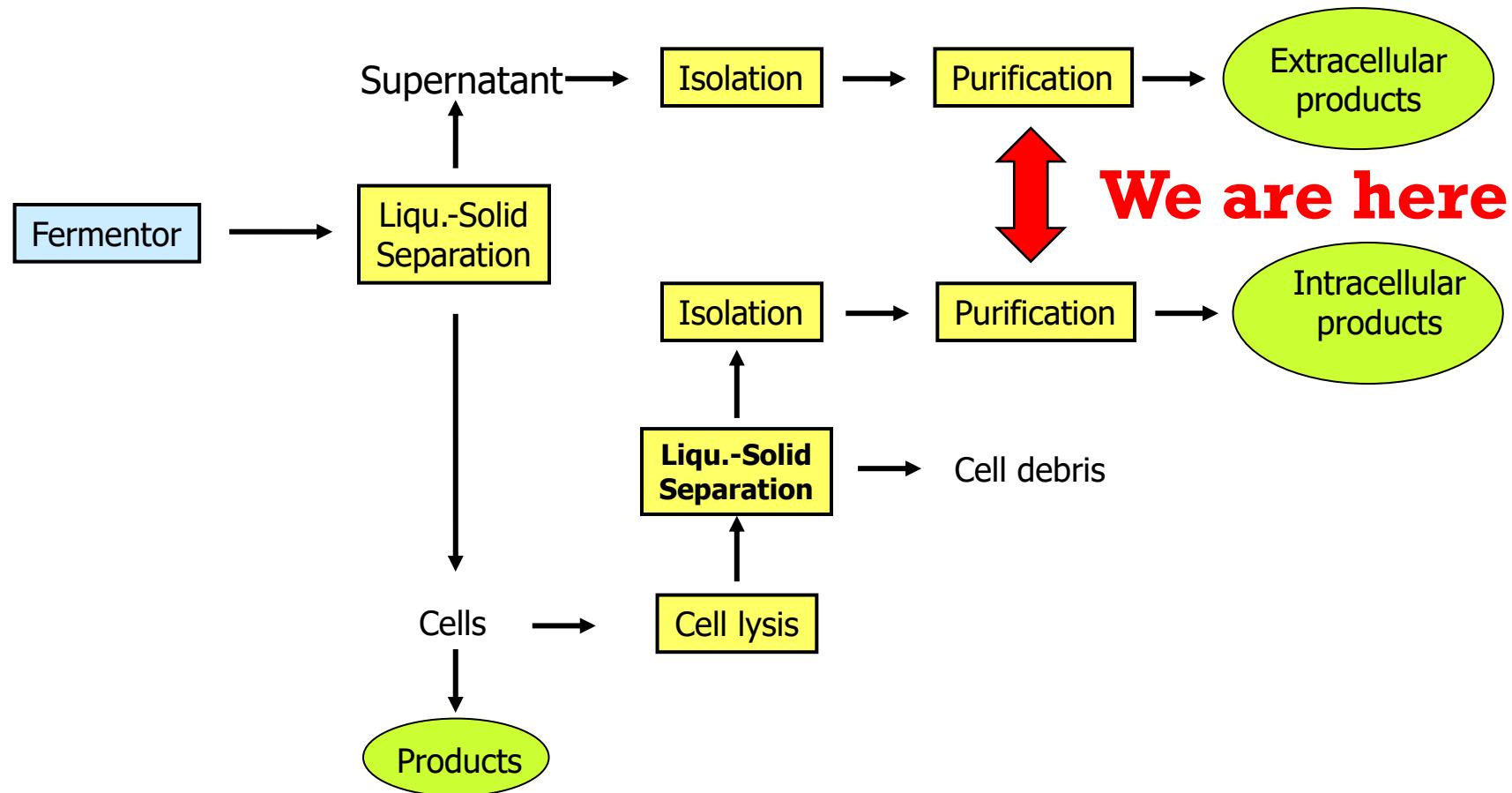




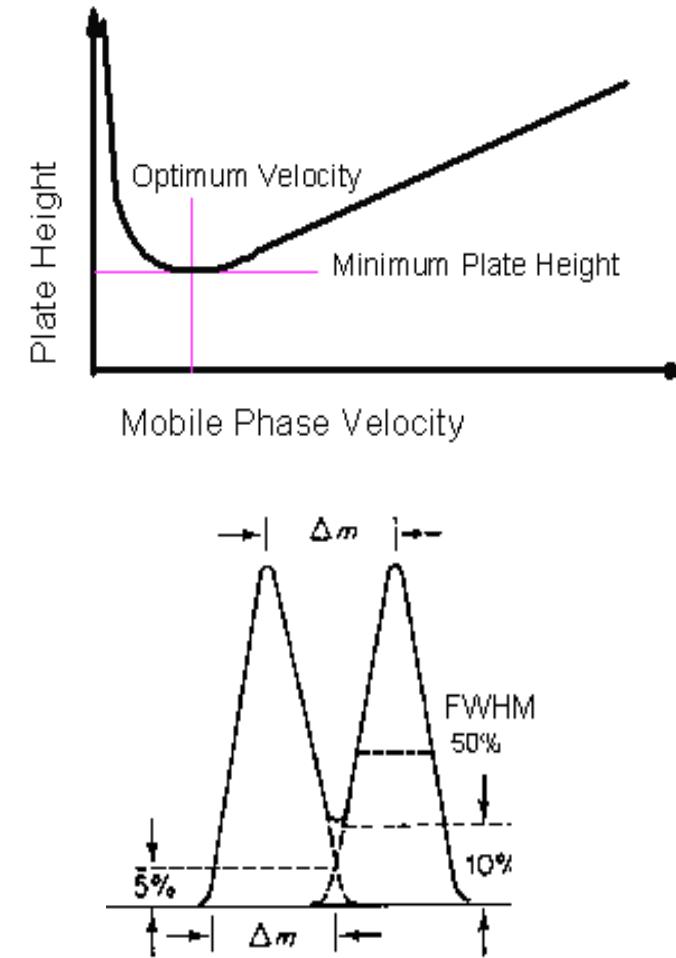
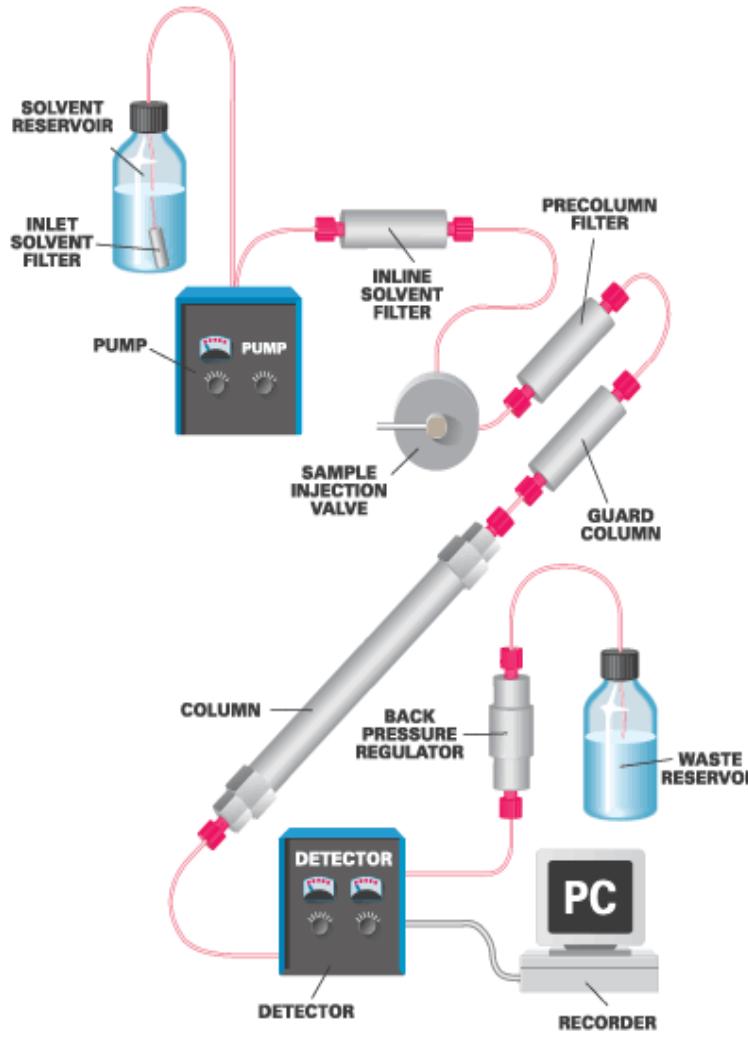
WARNING

- The theory of chromatographic separations spans over an extremely large number of topics ranging from the types of chromatographies, the design of the resins, the characterization of the column behavior, the optimization of the separation conditions etc ...
- We will limit ourselves to the most important of these subjects
- Here we will exclusively discuss **preparative chromatography**

Common pathway for a purification protocol



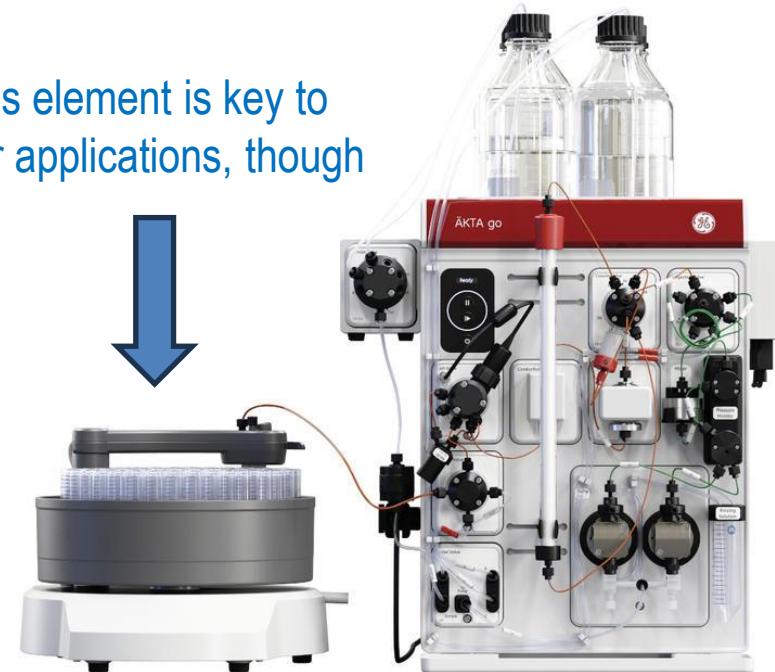
4.1 A quick reminder



Same components** are found in chromatographs at all scales

- Pumps
- Pipes, tubing, valves
- Injection/loading system
- Stationary phase
- Detector

This element is key to our applications, though



NB: the pictures are not to scale (far from it!)





A chromatogram conveys a lot of information

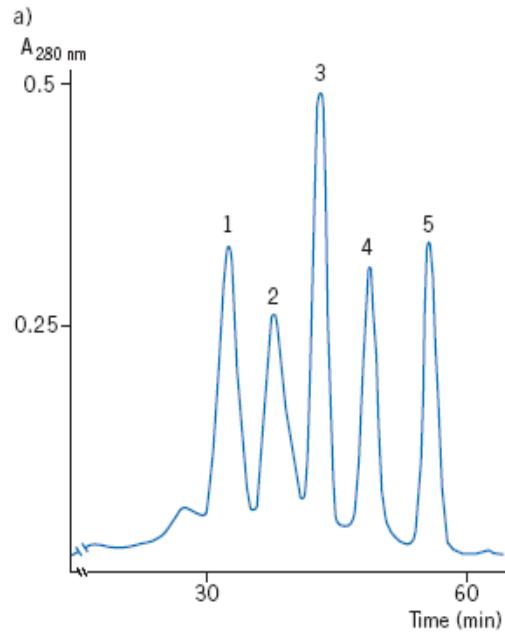
Column: Superose 6 HR 10/30

Sample: 100 μ l solution containing:

1. Thyroglobulin (M_r 669 000), 5 mg/ml
2. Ferritin (M_r 440 000), 0.3 mg/ml
3. Bovine serum albumin (M_r 67 000), 8 mg/ml
4. Ribonuclease A (M_r 13 700), 5 mg/ml
5. Glycyl tyrosin (M_r 238), 0.6 mg/ml

Buffer: 0.05 M phosphate buffer, 0.15 M NaCl, pH 7.0

Flow: 0.4 ml/min



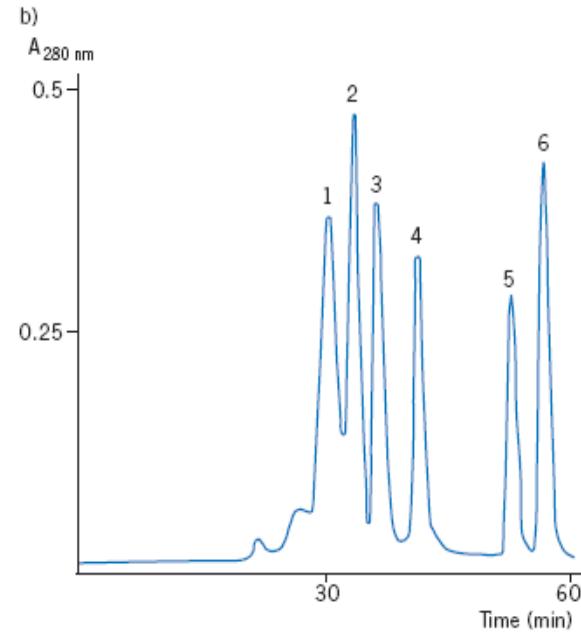
Column: Superose 12 HR 10/30

Sample: 100 μ l solution containing:

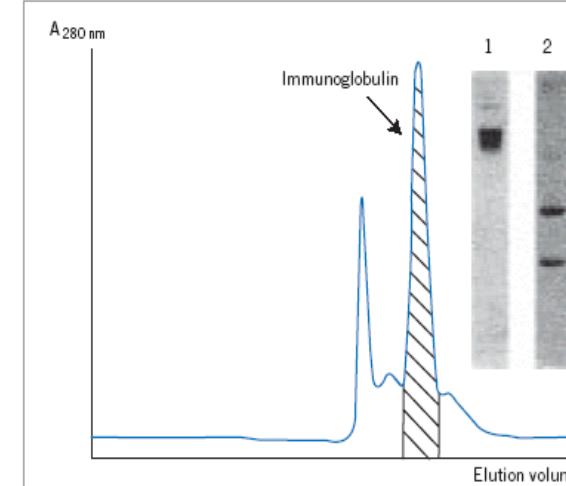
1. IgG (M_r 160 000), 2.5 mg/ml
2. BSA (M_r 67 000), 8 mg/ml
3. β -lactoglobulin (M_r 35 000), 2.5 mg/ml
4. Cytochrome C (M_r 12 400), 1 mg/ml
5. Vitamin B12 (M_r 1 355), 0.1 mg/ml
6. Cytidine (M_r 243), 0.1 mg/ml

Buffer: 0.05 M phosphate buffer, 0.15 M NaCl, pH 7.0

Flow: 0.4 ml/min



However, **identification** of the peak corresponding to the target molecule requires some specific analytical method



Sample: IgG fraction from previous ion exchange step (sample volume equivalent to 1% of V_t . (V_t = column volume))

Column: BP 113/120 containing Sephadryl S-200 HR, bed height 100 cm

Buffer: 0.05 M Tris-HCl, 0.15 M NaCl, pH 7.5

Flow: 7.5 cm/h

Fig. 34. Purification of monoclonal antibodies on Sephadryl S-200 HR. Inset shows analysis by gradient SDS-PAGE of the immunoglobulin pool. Lane 1, native sample; lane 2, sample reduced with 2-mercaptoethanol.

Production-scale columns



Importance of column packing

- The quality of column packing is key to the separation efficiency
- Beads should be distributed in a highly homogenous manner and the bed should be devoid of cracks and channels
- Packing can be done manually for lab-scale columns, but has to be automatized for production-scale systems
- There are several experimental techniques to assesss the quality of a packing. For instance, breakthrough curves or pulse injection of an inert tracer.
- In a well-packed column, the height of a theoretical plate H is about 3 times the diameter of the resin particles.

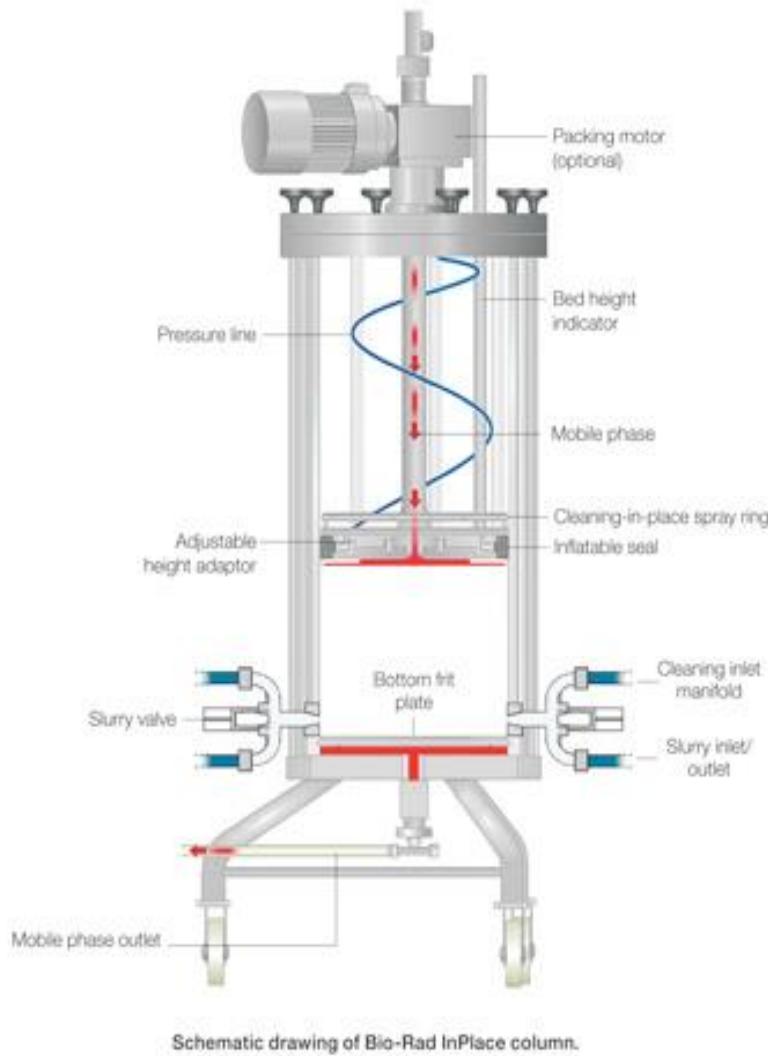


Source: <https://biopharma-asia.com/>

A brief check list (before you do anything stupid)

- **Industrial chromatography columns** are usually not stored for extended periods
- They have to be filled with resin and packed on a regular basis
- It is then important to assess the **quality of the packing** before starting any purification campaign
- Parameters that are typically measured include **pressure drop**, **peak symmetry** (or lack thereof) and **number of theoretical plates (NTP)**
- Please check the **Bio Rad video** on the **packing of industrial columns**

4.2 Column filling and packing

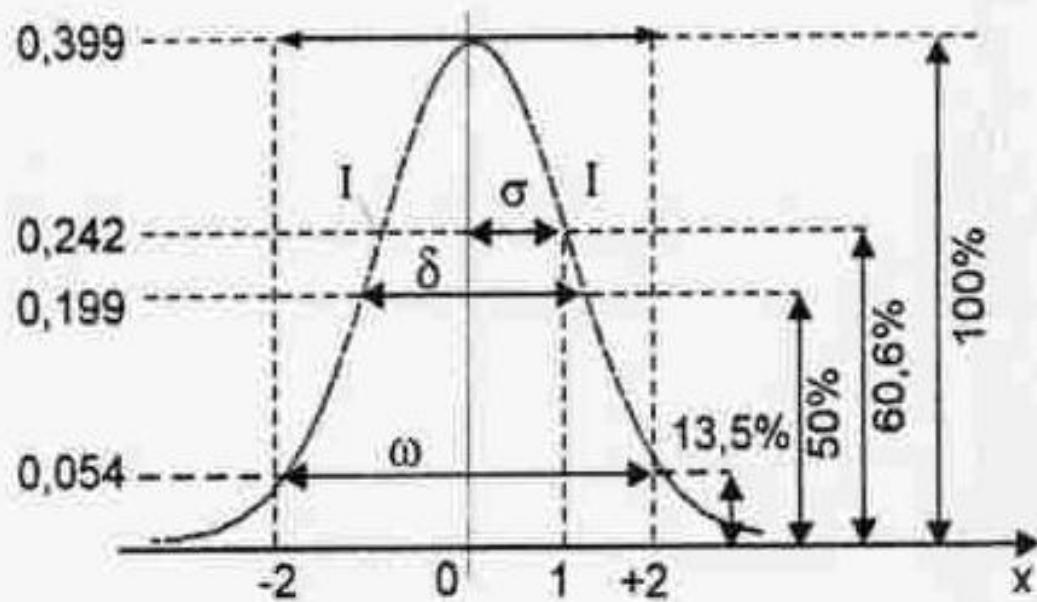


BIO-RAD

Vidéo sur le
remplissage de
colonnes industrielles



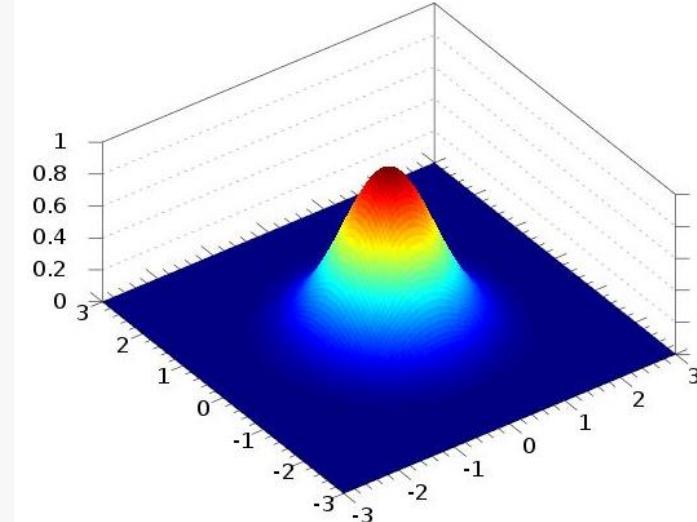
Properties of Gaussian peaks



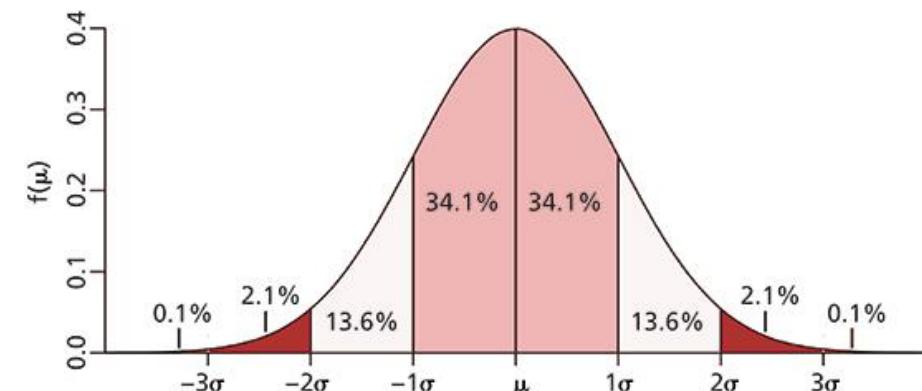
$$\begin{aligned}\delta &= 2,35 \sigma \\ \omega &= 4 \sigma \\ \omega &= 1,7 \delta\end{aligned}$$

(6.4-1)

l'aire comprise entre -2 et +2
vaut 95,4% de l'aire totale
comprise entre la courbe et
l'axe des x



- σ is the standard deviation
- σ^2 is the variance





Number N and equivalent height H of theoretical plates

Theoretical Plates

$$N = 5.54 \left(\frac{t_r}{W_{1/2h}} \right)^2$$
$$N = 16 \left(\frac{t_r}{W_b} \right)^2$$

$$N = \frac{t_r^2}{\sigma^2} \quad (6.4-2)$$

$$N = 5.54 \cdot \left(\frac{t_r}{W_{0.5h}} \right)^2 = 16 \cdot \left(\frac{t_r}{W_{base}} \right)^2 \quad (6.4-3)$$

- There are various ways to calculate N from the peak geometry. They all derive from Equ. 6.4-1
- The formulas of equation 6.4-3 are most often used

The number of theoretical plates is an expression of the quality of the column packing and the homogeneity of the flow through it.

The peak is obtained by injecting a small amount of a tracer that does not interact with the chromatography resin.

$$H = L/N \quad (6.4-4)$$

The equivalent height of a theoretical plate, H, corresponds to the total column length, L, divided by N



Peak asymmetry F_a and resolution R

- Various factors (inhomogenous packing, channelling) can change the peak appearance into a non-Gaussian geometry
- The observed asymmetry is characterized by two parameters, each of them measured at 10 % of peak height:

The **resolution R** is an expression of how efficient the separation is between two components

$$R = 2 \cdot \frac{t_2 - t_1}{W_1 + W_2}$$

Asymmetry factor $F_a = \frac{B}{A}$ (6.4-5)

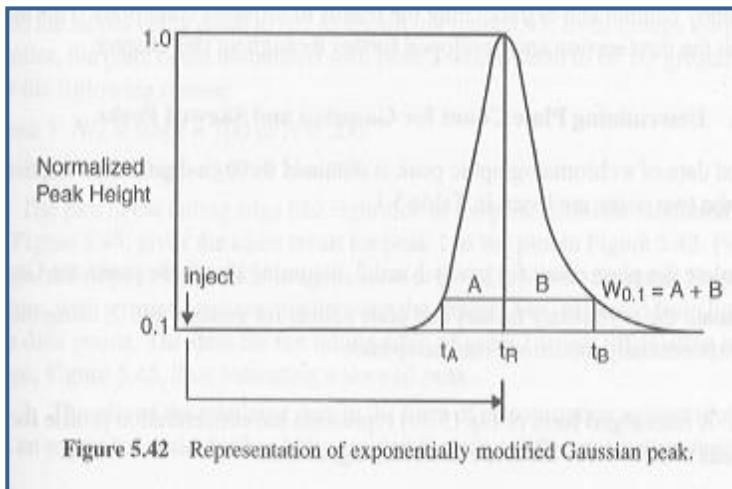
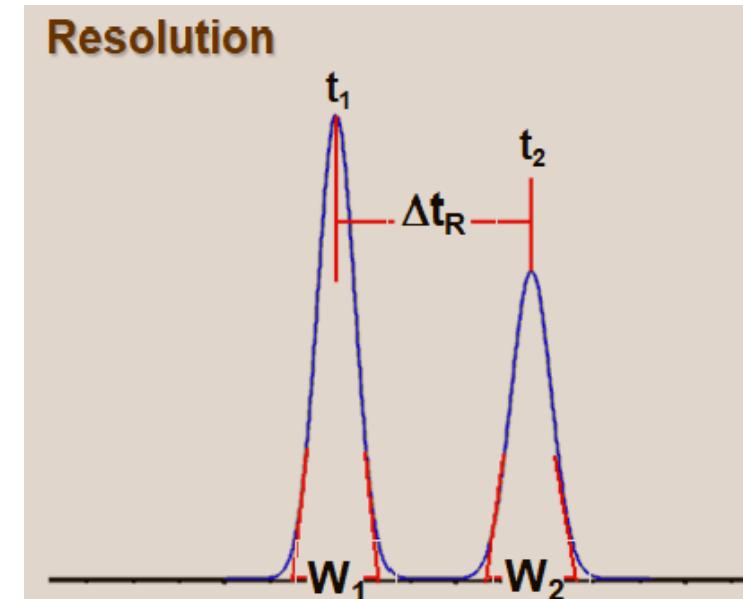
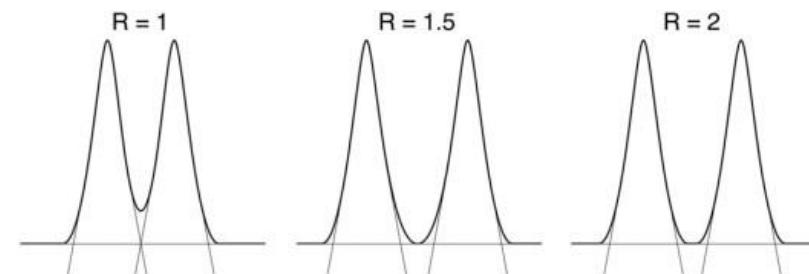
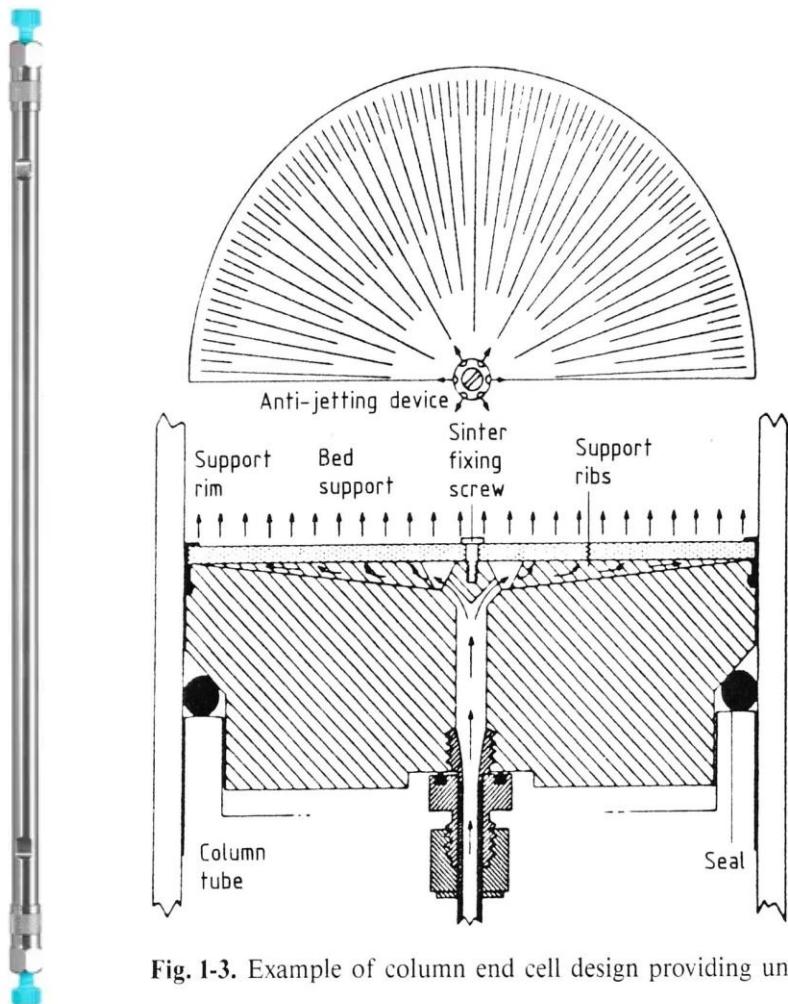


Figure 5.42 Representation of exponentially modified Gaussian peak.

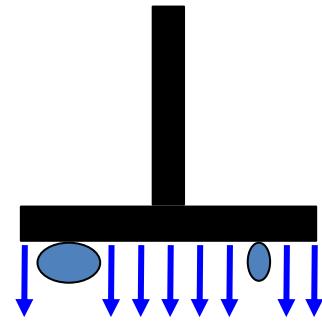


Influence of the liquid distribution system

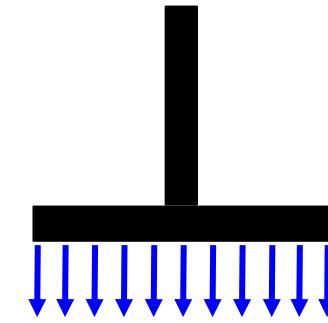
HPLC column: one entry point but small diameter: no liquid distribution issue



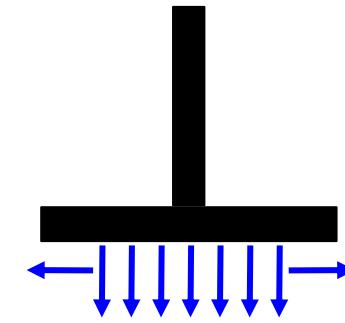
Trapped bubbles



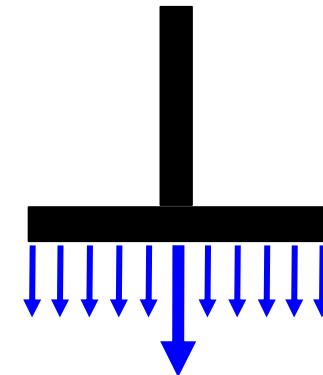
Even distribution



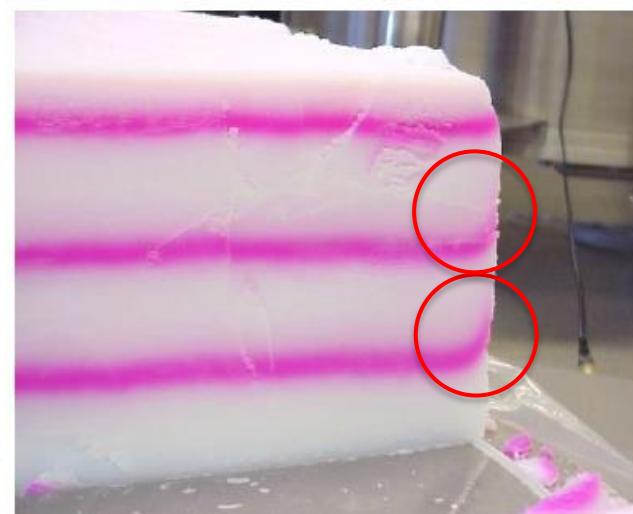
Wall effects



Liquid jetting



Wall Effect



Liquid jetting

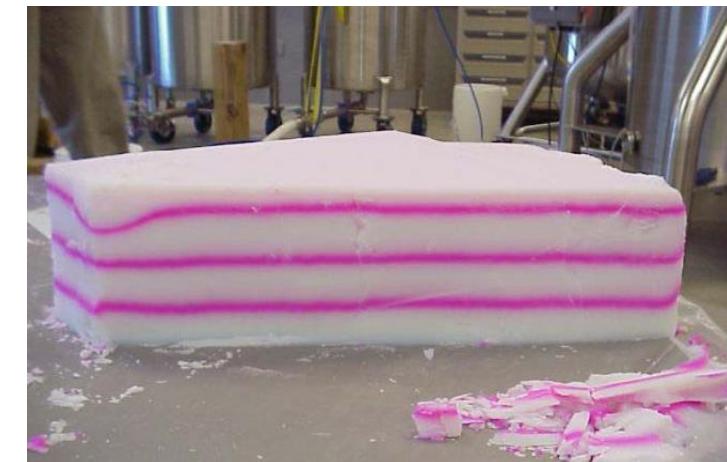


Fig. 1-3. Example of column end cell design providing uniform flow distribution.

Packing quality: number of theoretical plates, peak (a)symmetry

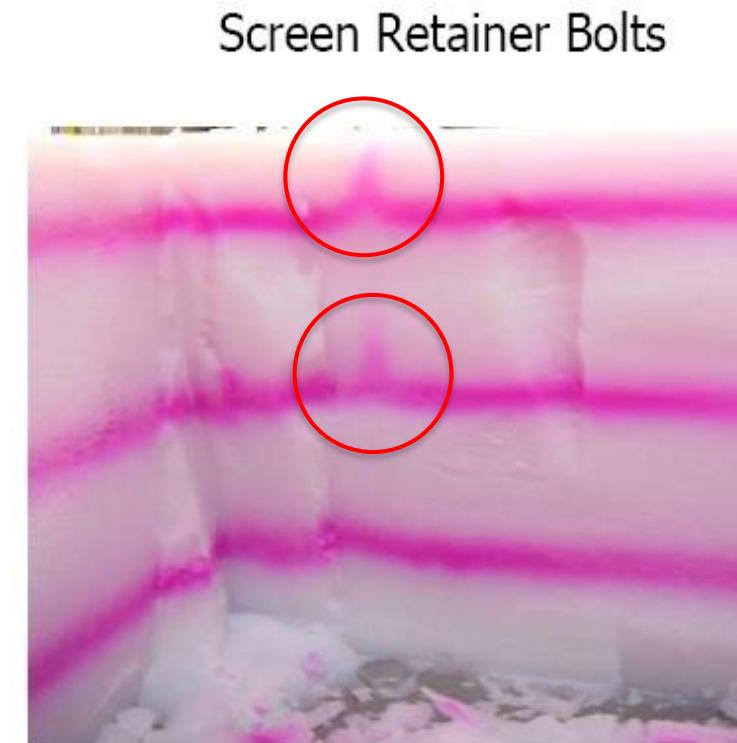
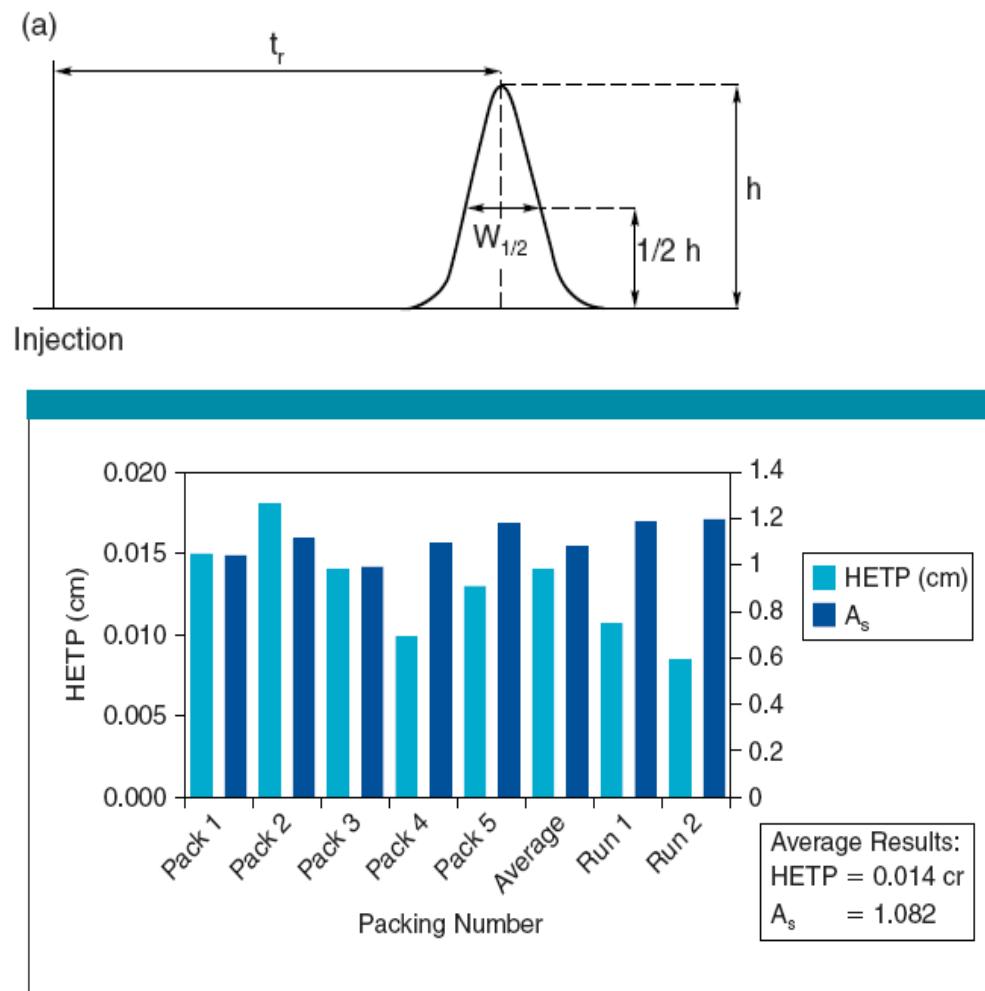
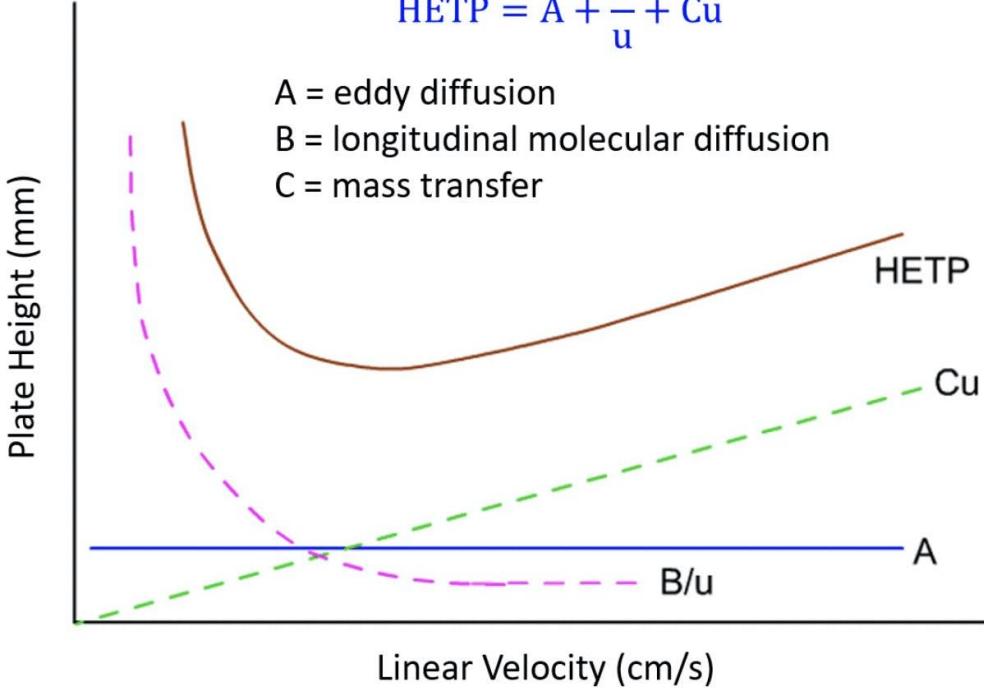


Figure 2. Summary of Sephadex S-200 HR packing qualification

The van Deemter equation

$$H = A + \frac{B}{u} + C \times u$$

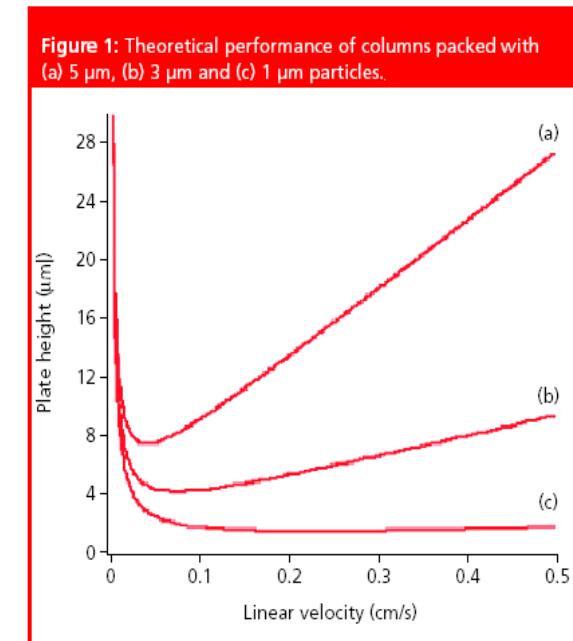


Beware!

1. The van Deemter equation is valid only for an isocratic elution of the solutes
2. Although it leads to lower H values, one cannot decrease the resin particle size indefinitely because of the corresponding increase in pressure drop

In protein chromatography,
the C term rules!!!

- The van Deemter equation illustrates the difficulty to combine a low value for H (efficient separation) with a high flow rate/liquid velocity
- The A, B and C terms of the equation are related to packing quality, axial diffusion and mass transfer, respectively



Effect of flow rate and loading on resolution (in protein chromatography)

Column: SOURCE 30Q, 10 mm i.d. x 50 mm (4 ml)

Sample: Mixture of lactoglobulin B and amyloglucosidase

Sample load: 1 mg/ml bed volume

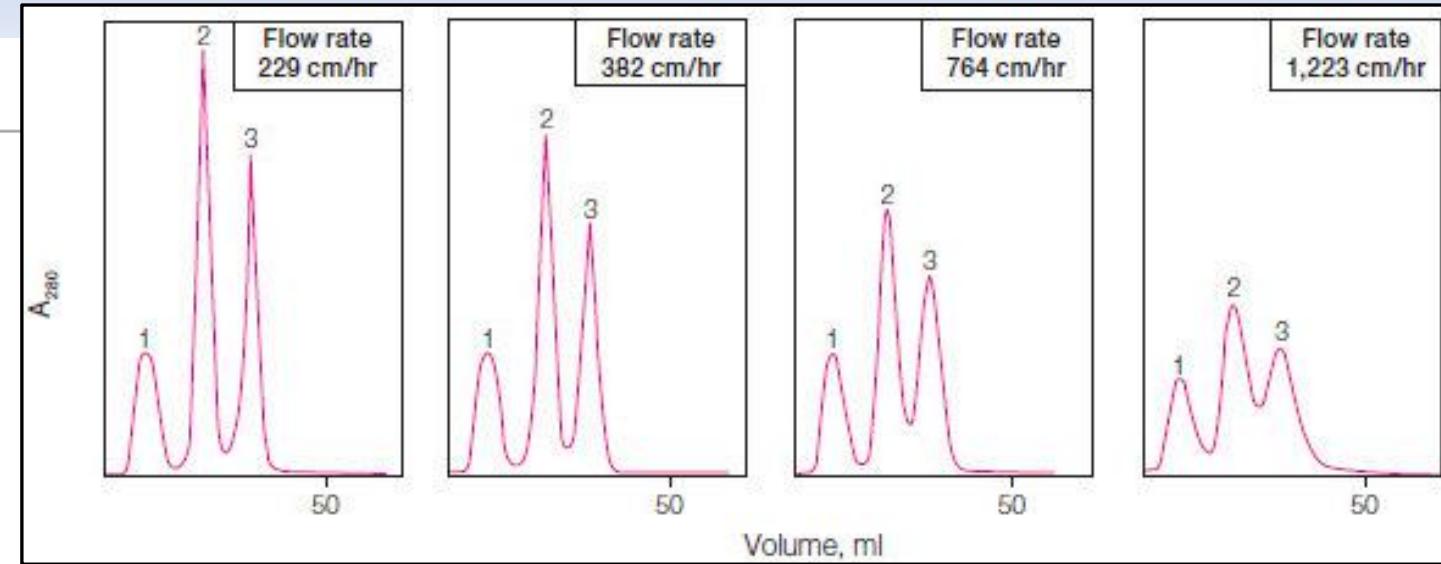
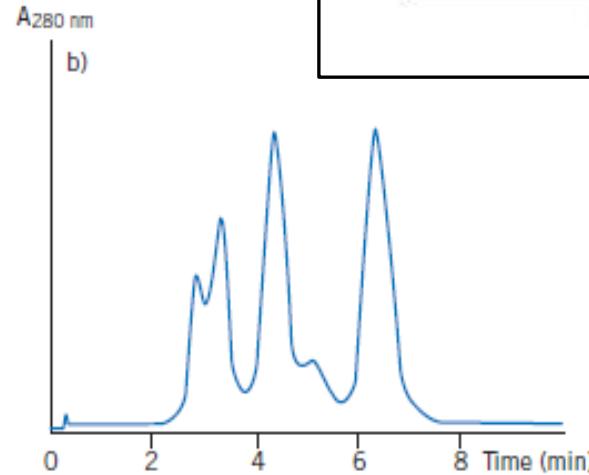
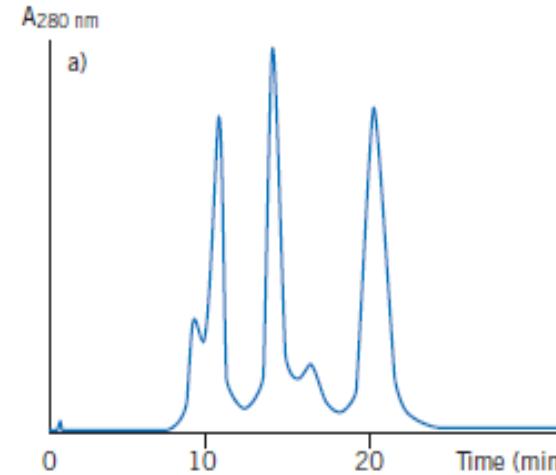
Start buffer: 20 mM BIS-TRIS PROPANE, pH 7.0

Elution buffer: 0.5 M sodium chloride, 20 mM BIS-TRIS PROPANE, pH 7.0

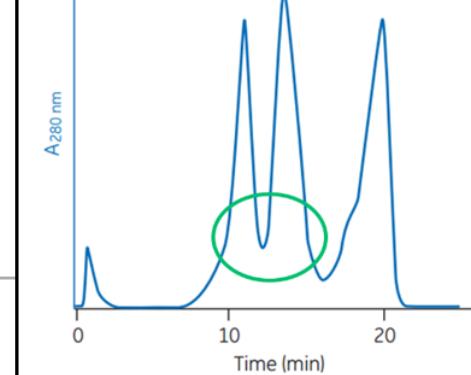
Flow: a) 4 ml/min (300 cm/h)

b) 13 ml/min (1000 cm/h)

Gradient: 0–100% elution buffer, 20 CV



(A) Sample load: 10 mg
Column: SOURCE™ 30S, 5 mm x 50 mm (i.d. x h)



(B) Sample load: 1 mg
Column: SOURCE 30S, 5 mm x 50 mm (i.d. x h)

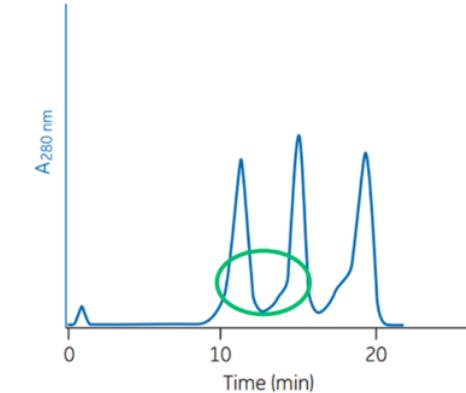


Fig. 26. Influence of increasing flow rate on resolution.

Source: Cytiva